

SBR – System Overview



- ☐ **Overview of SBR System**
- ☐ **Design Considerations for SBR System**
- ☐ **Recommended design parameters**
- ☐ **Advantage / Disadvantage of SBR**
- ☐ **Variation of SBR Systems**

Historical Prospective:

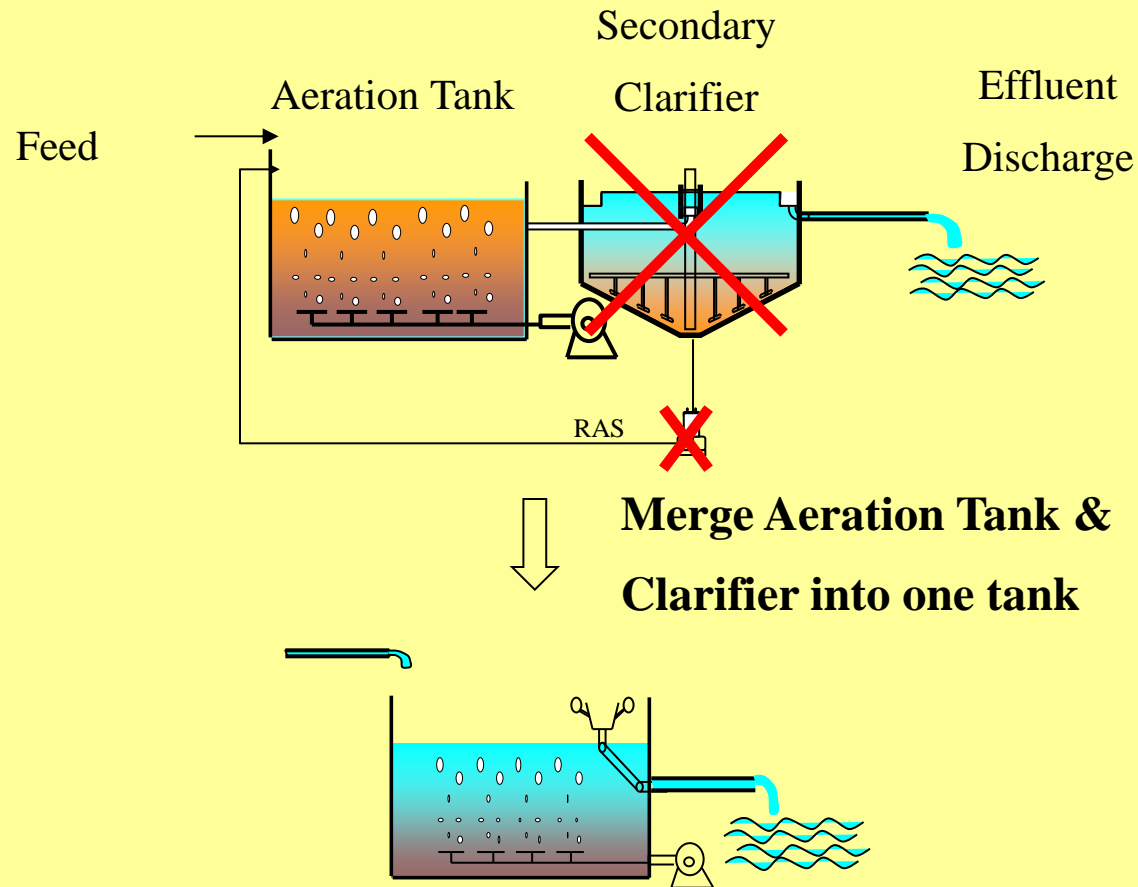
- Fill and draw first shown beneficial use - Arden and Lockett in England.
- Many difficulties associated with “batch” processes, continuous flow become popular.
- Resurgence of “batch”:
 - when Pasveer’s modification of OD to intermittently aeration and discharge;
 - Goronszy’s use of continuous feed and intermittently aeration and discharge.

Today’s prospective:

- Hardware devices controllable: motorized / pneumatic valves, motorized shaft, etc.;
- Advent of PLC making operator’s control: automated;

Batch processes - popular again due to many difficulties resolved and benefits demonstrated.

Sequencing Batch Reactor **merges** aeration & clarifier:



SBR (Sequencing Batch Reactor):

- Sewage feeds to a reactor, biological oxidation and clarification take place at same reactor
- Operated on alternative sequence of cyclical mode.
- There are five (5) basic sequences in a cycle, namely:
 - Fill
 - React (Aeration)
 - Settle
 - Decant
 - Idle (optional- mostly not use)

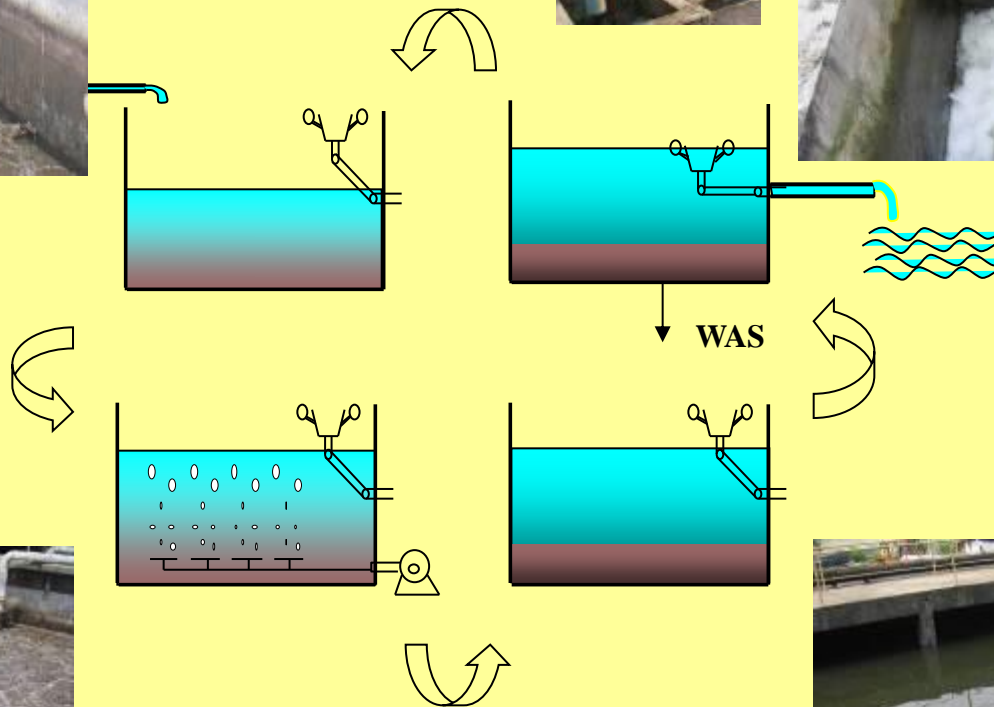
SBR System



(1) Fill



(4) Decanting



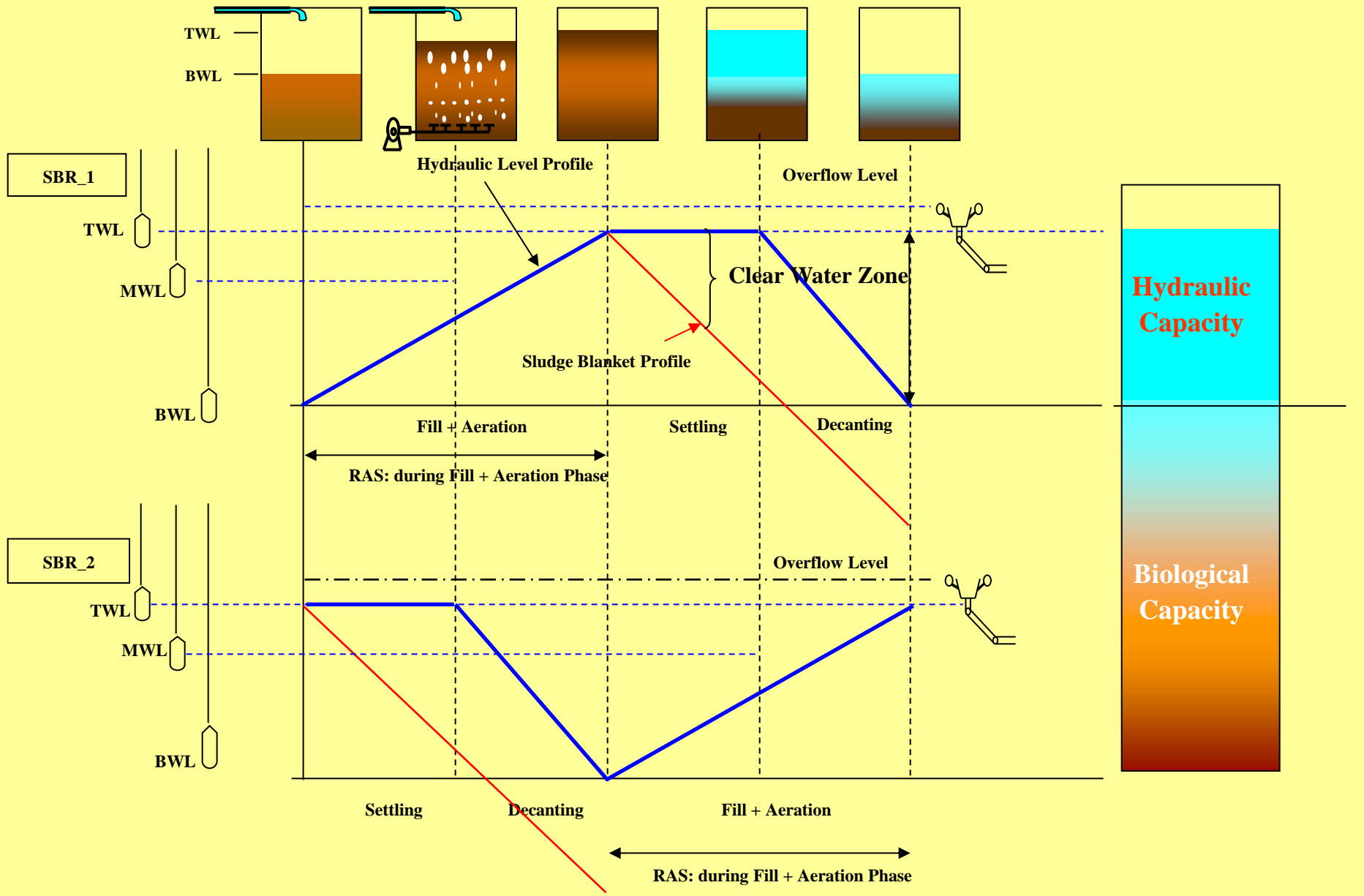
(2) React

(3) Settle



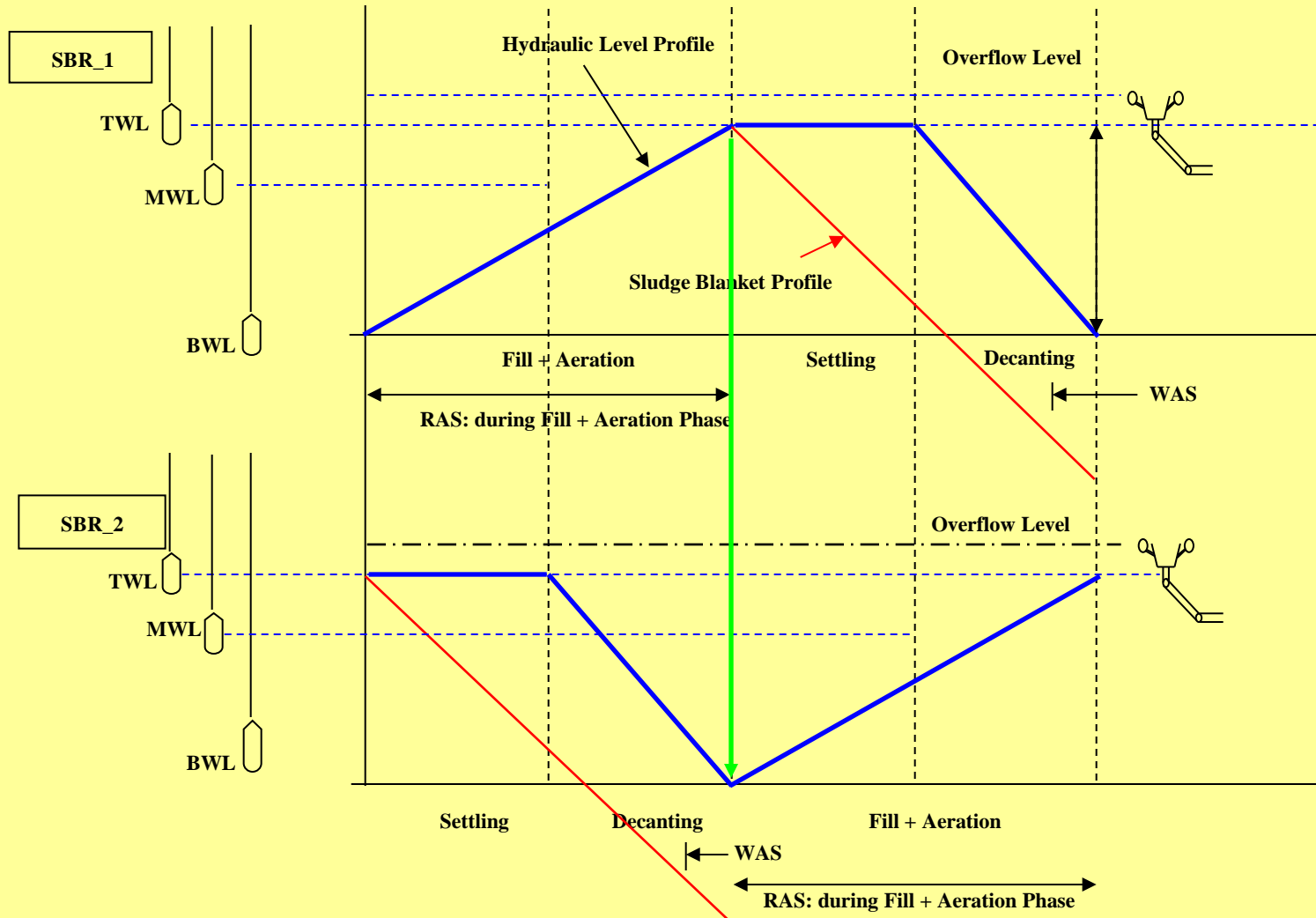
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SBR Cycle: Hydraulic & Sludge Profile

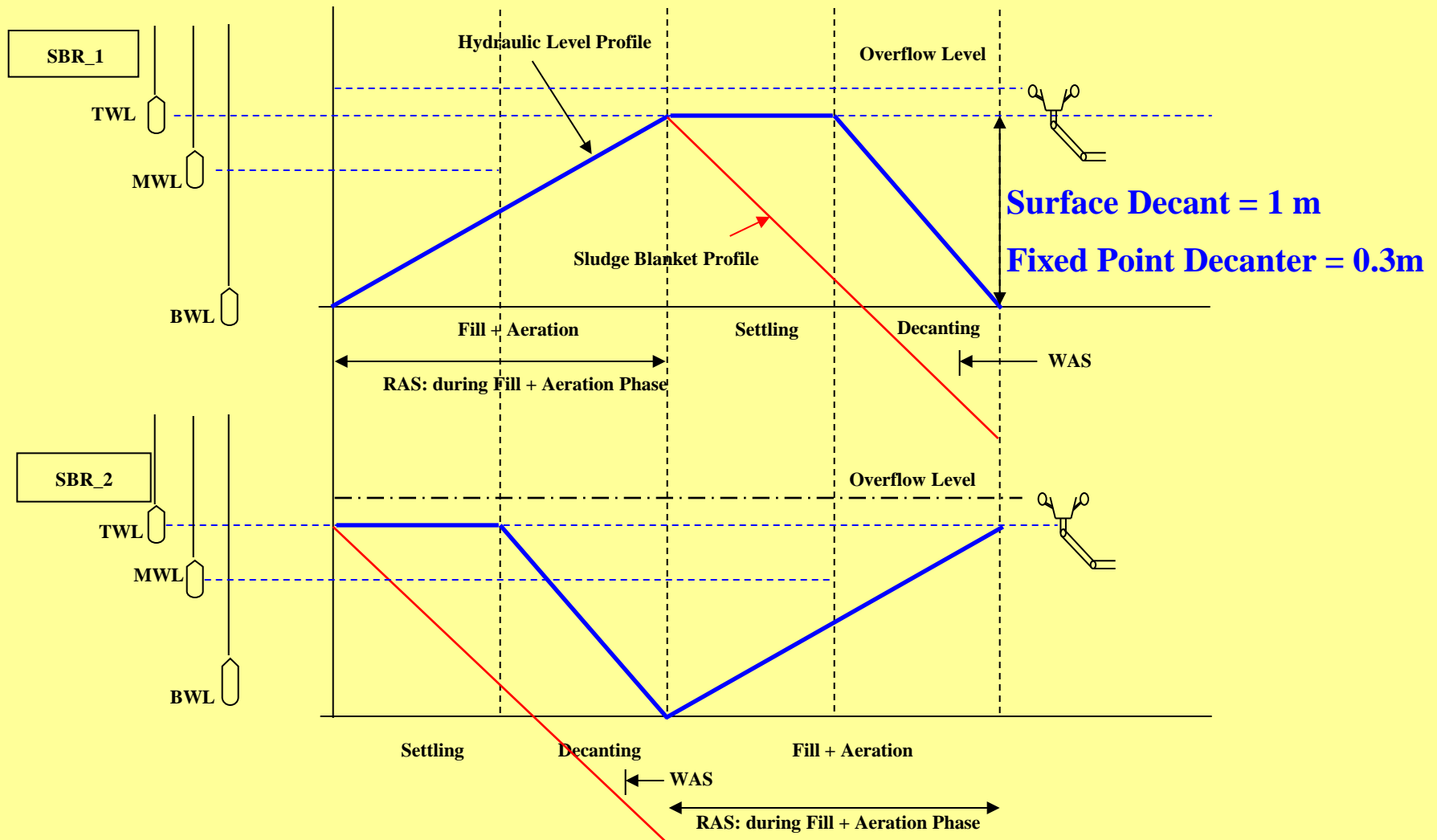


SBR Cycle: Hydraulic & Sludge Profile

$$N_{SBR} = t_{\text{cycle}} / t_{\text{fill}}$$



SBR Cycle: Hydraulic & Sludge Profile



SBR Cycle: Hydraulic & Sludge Profile

Correlation of Zone Settling Velocity with MLSS & SVI

Correlation of V_i and MLSS based on work and studies by Daigger 1993 and Wahlberg, 1995

$$\ln(V_i) = 1.87 - (0.1646 + 0.001586 \times \text{SVI}) X_t$$

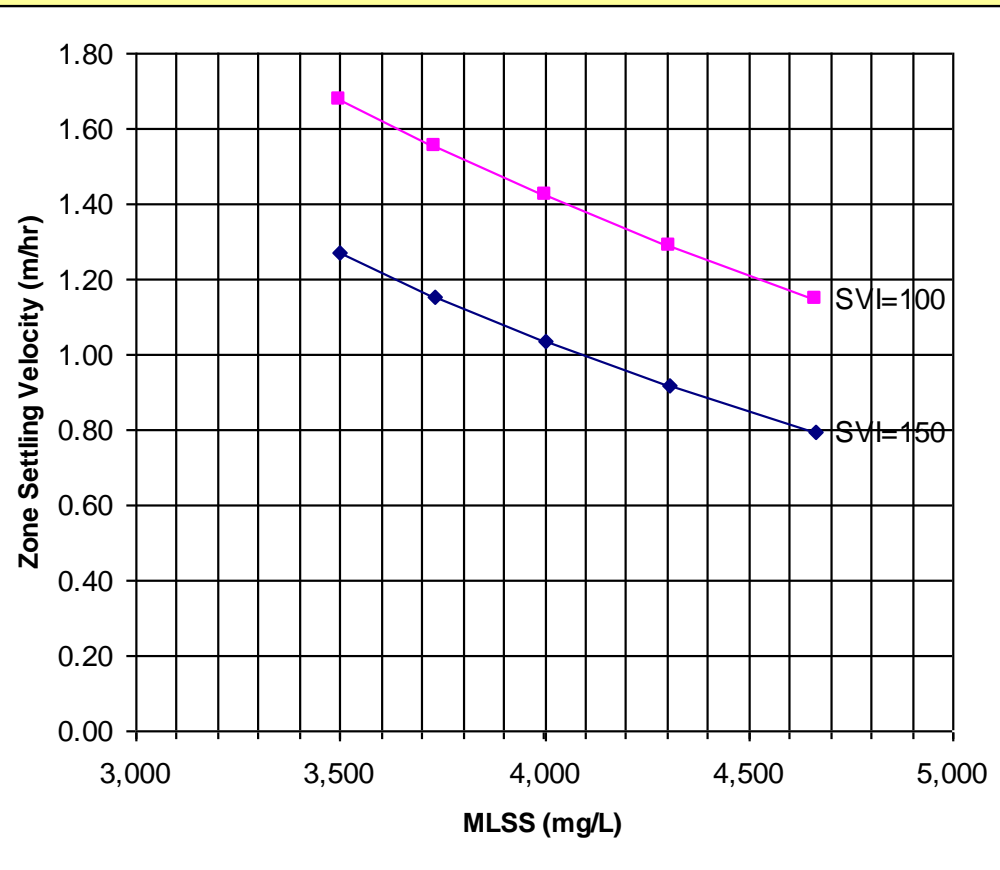
$$V_{\text{design}} = V_i / (\text{SF}=1.25)$$

where:

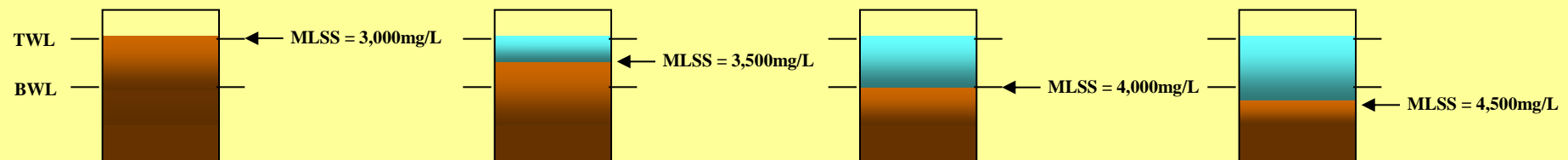
V_i = Zone settling velocity or interfacial settling velocity (m/hr)

SVI = Sludge Volume Index, (mL/g)

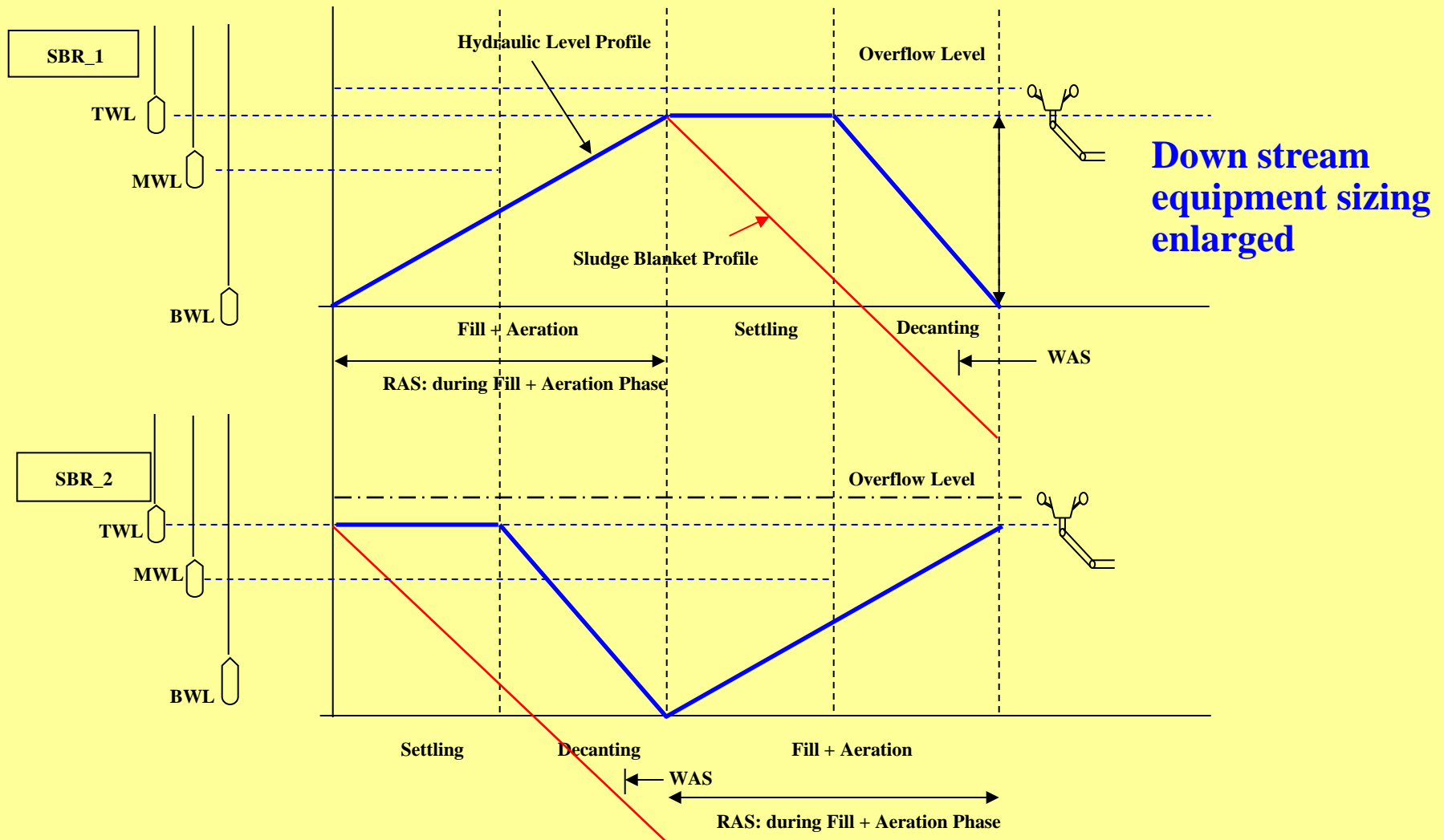
X_t = MLSS concentration, (g/L)



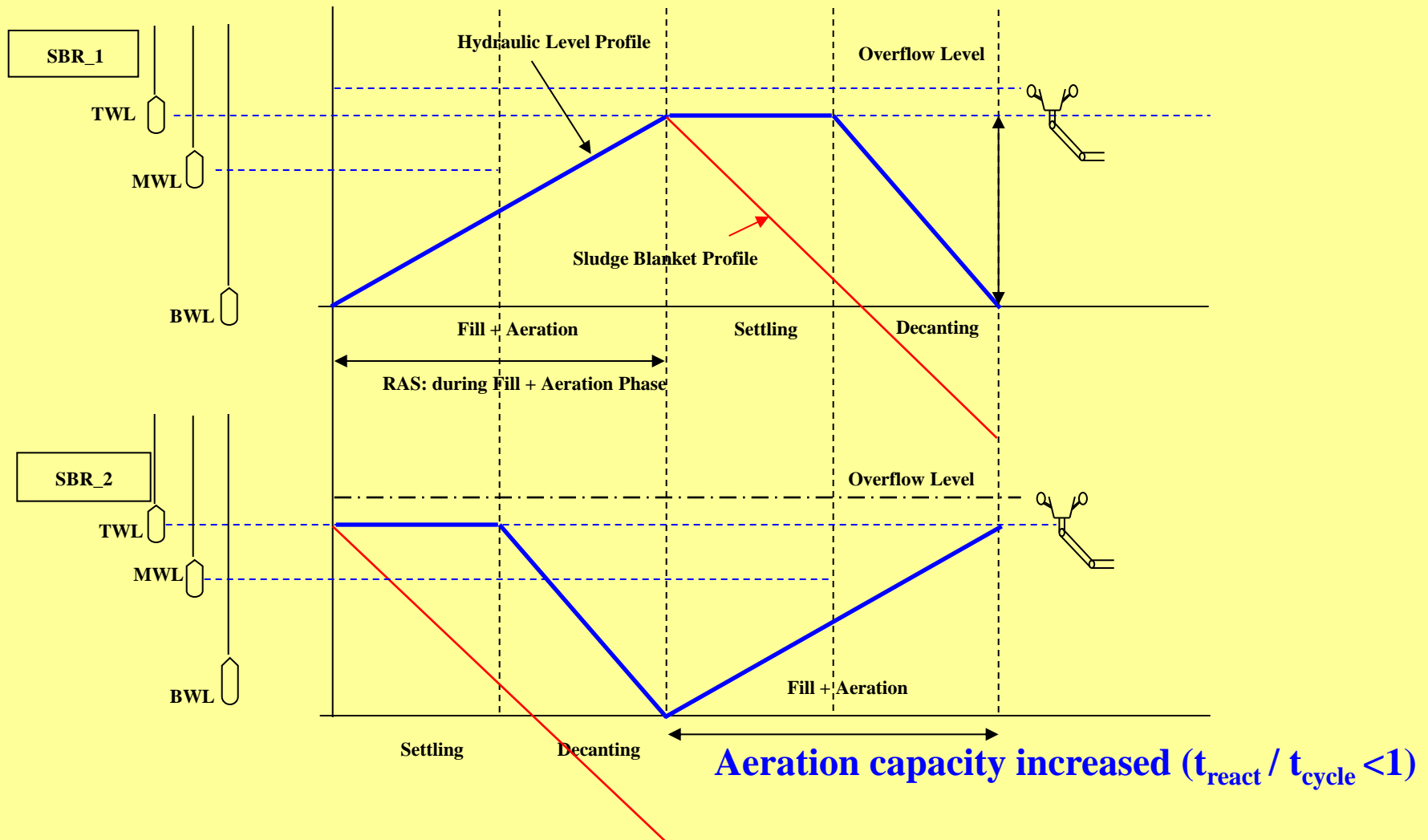
MLSS at TWL = 3,000 mg/L



SBR Cycle: Hydraulic & Sludge Profile



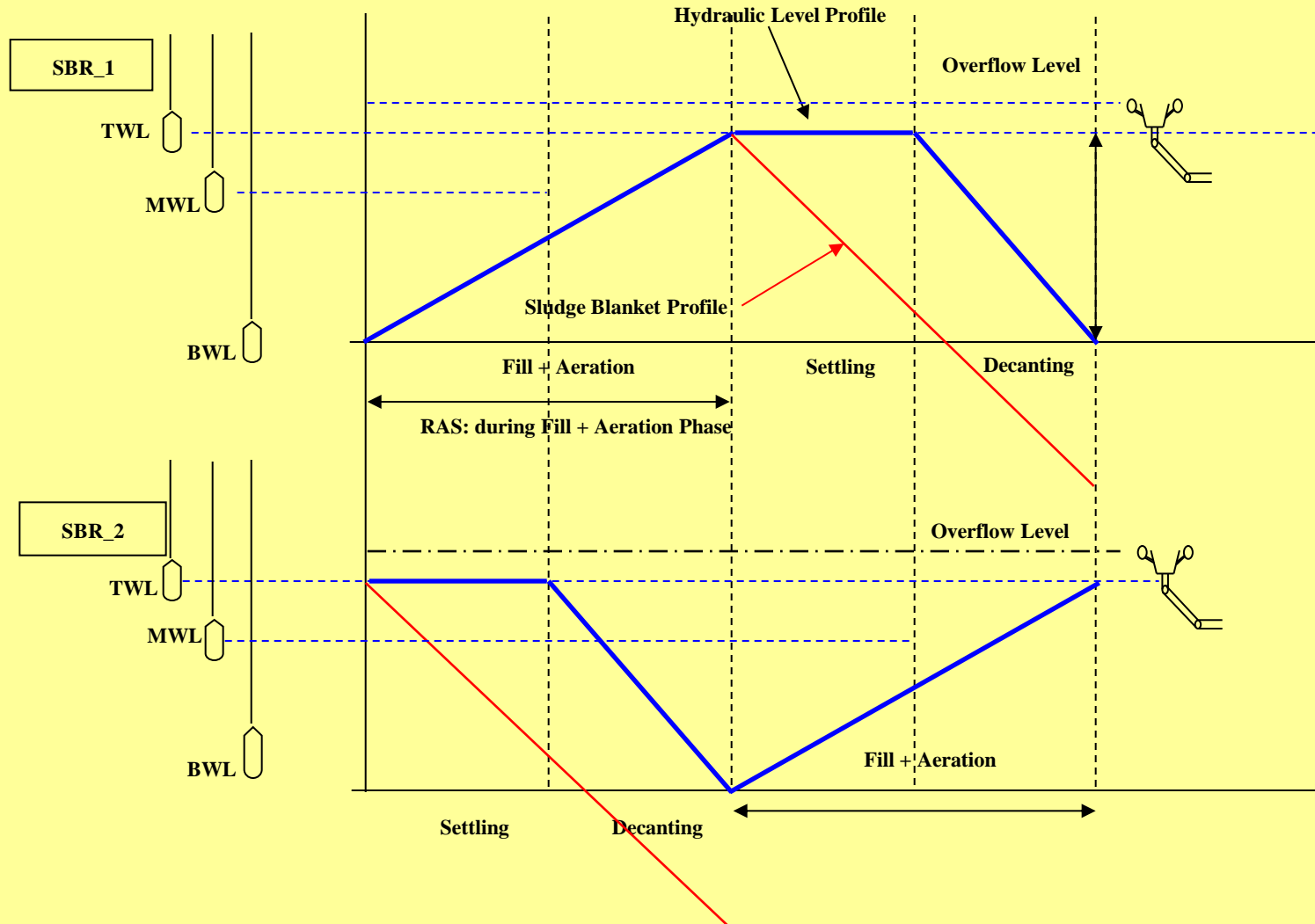
SBR Cycle: Hydraulic & Sludge Profile



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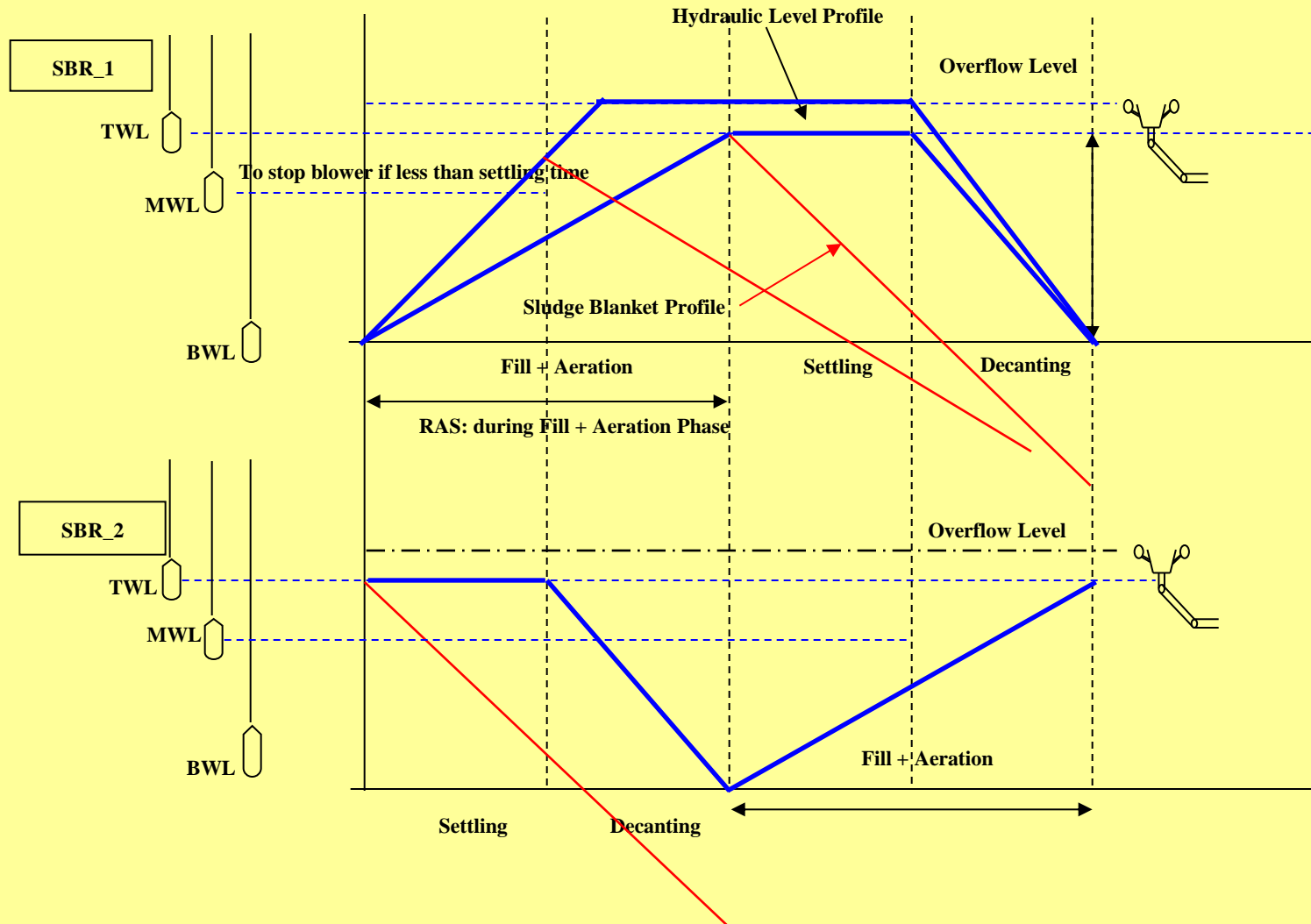
$$N_{\text{cycle}} \text{ (cycle/day)} = 24 \text{ (hr/day)} / \Sigma t_{\text{cycle}} \text{ (hr/cycle)}$$

Preferably unique round number for each SBR Tank



SBR Cycle: Hydraulic & Sludge Profile

High Flow: Need to stop aeration: allow settling earlier



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Recommended Design Parameters



Syarikat Pembetungan Nasional Anda

Your National Sewerage Company

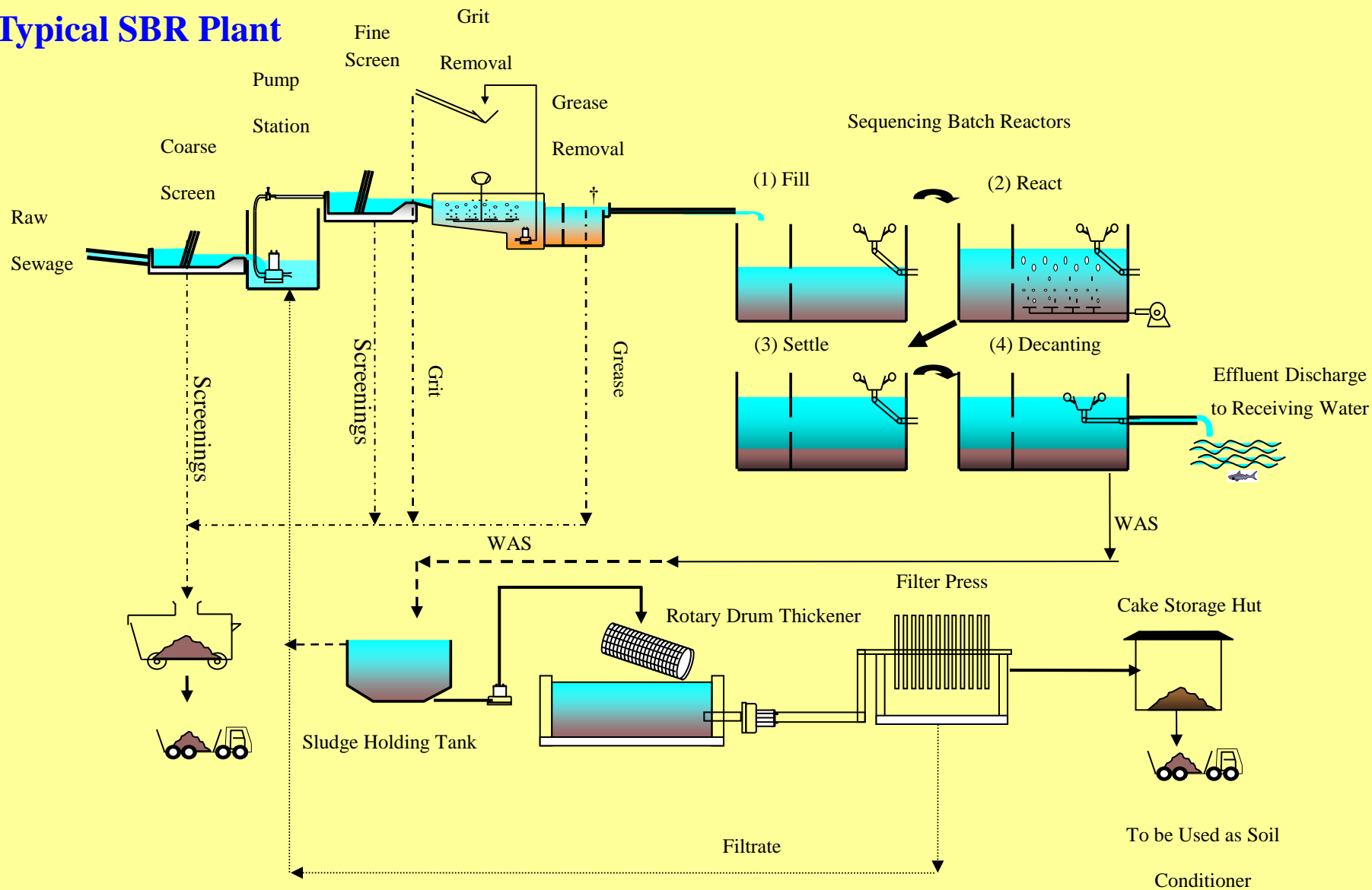
Parameter	Unit	Continuous Fill and Intermittently Decant	Intermittently Fill and Intermittently Decant
No. of Reactors	Unit	Minimum 2	Minimum 2
Hydraulic retention time at Qavg (at average water level)	hr	18 – 24	18 – 24
F/M Ratio	d ⁻¹	0.05 – 0.08	0.05 – 0.30
Sludge Age	D	20 – 30	10 – 30
Sludge Yield	kg sludge/ kg Load	0.75	0.75
MLSS (End of Decant)	mg/L	3,000 – 4,500	3,000 – 5,000
Cycle Time	Hr	4 – 8	4 – 8
Oxygen Required DO (Reactor) DO (Effluent)	mg/L mg/L	0 ~ 6.5 2.0	0 ~ 6.5 2.0
Minimum Settling Time (before start of decant)	Hr	> 0.6 for decant from TWL downward > 1.0 for fixed points decant	> 0.6 for decant from TWL downward > 1.0 for fixed points decant
Decant Time	Hr	≥ 1.0	≥ 1.0
Decant Depth	M	Max 1.0 (surface decant only)	max 1.5 (surface decant only)
Decant Volume	%	Not more than 25% of volume of Biological Reactor at TWL	Not more than 30% of volume of Biological Reactor at TWL
Decanting Device Loading Rate*	m ³ /m/hr	≤ 20 for decant from TWL & if SOR(decant) <20 m ³ /m ² .d ≤ 15 for decant from TWL & if SOR(decant) <30 m ³ /m ² .d ≤ 10 for fixed points decant regardless of SOR	≤ 20 for decant TWL & if SOR(decant) <20 m ³ /m ² .d ≤ 15 for decant from TWL & if SOR(decant) <30 m ³ /m ² .d ≤ 10 for fixed points decant regardless of SOR
WAS	Kg Sludge/d	$WAS = \frac{\text{Total Solids in System}}{\text{Sludge Age}}$	$WAS = \frac{\text{Total Solids in System}}{\text{Sludge Age}}$
Fill Volume	m ³	$V_{\text{fill}} = (Q_P \text{ m}^3/\text{hr} \times 1.5\text{hr}) + (T_{\text{fill}} - 1.5) \times Q_{\text{AVG}}$ (if no EQ) $V_{\text{fill}} = Q_{\text{AVG}} \times T_{\text{fill}}$ (if preceded by EQ)	$V_{\text{fill}} = (Q_P \text{ m}^3/\text{hr} \times 1.5\text{hr}) + (T_{\text{fill}} - 1.5) \times Q_{\text{AVG}}$ (if no EQ) $V_{\text{fill}} = Q_{\text{AVG}} \times T_{\text{fill}}$ (if preceded by EQ)

SBR System



Syarikat Pembetungan Nasional Anda
Your National Sewerage Company

Typical SBR Plant



Construction Cost

Year (Construction)	Unit	2002	2000	2000	2001
Size	(in PE)	50,000	20,000	15,500	12,000
Flow	(m ³ /d)	11,250	4,500	3,488	2,700
Total Cost	(RM in Million)	4.80	3.40	3.52	2.36
C&S Cost (exclude Pilling)	(RM in Million)	2.47	1.64	1.72	0.94
M&E Cost	(RM in Million)	2.33	1.76	1.80	1.42
Cost / PE	(RM/PE)	96	170	227	197
Cost / m³	(RM/m ³)	207	391	516	526

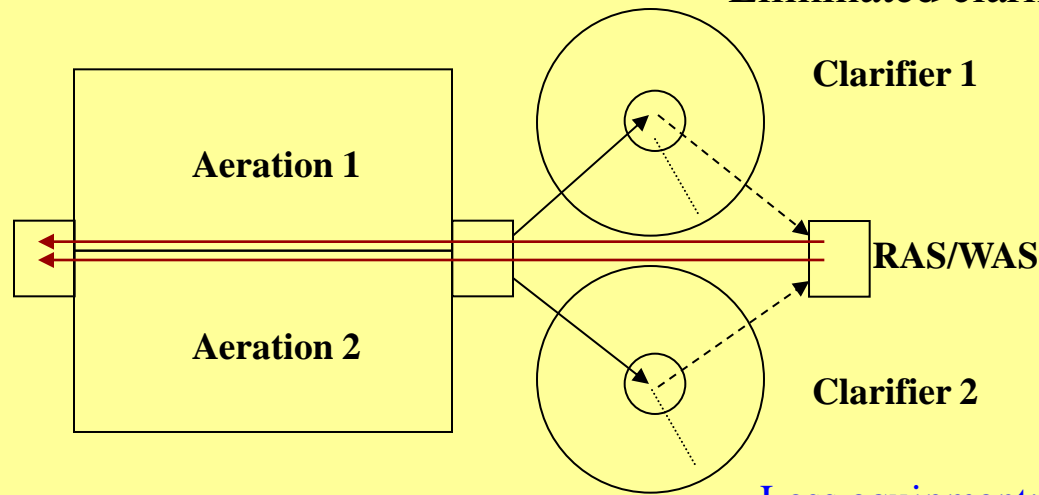
Electricity Cost

Size	(in PE)	<5,000	<10,000	<20,000	<50,000
Electricity	(RM/PE/yr)	8.73	3.03	1.48	1.66

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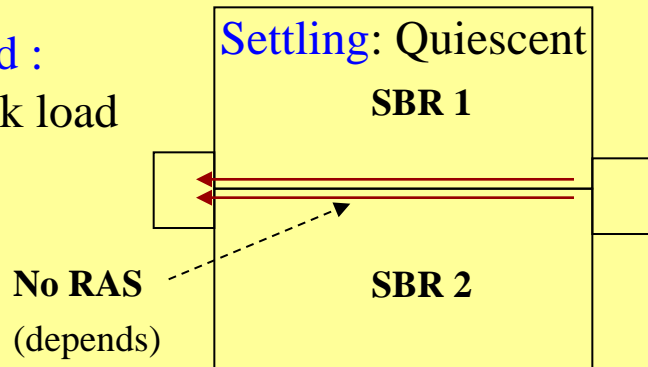
SBR advantages

Smaller land area requirements:
Eliminated clarifiers



Less equipment: No scrapper

Batch feed :
Less shock load



Multi-Process operation in one tank:

Nitrification / Denitrification

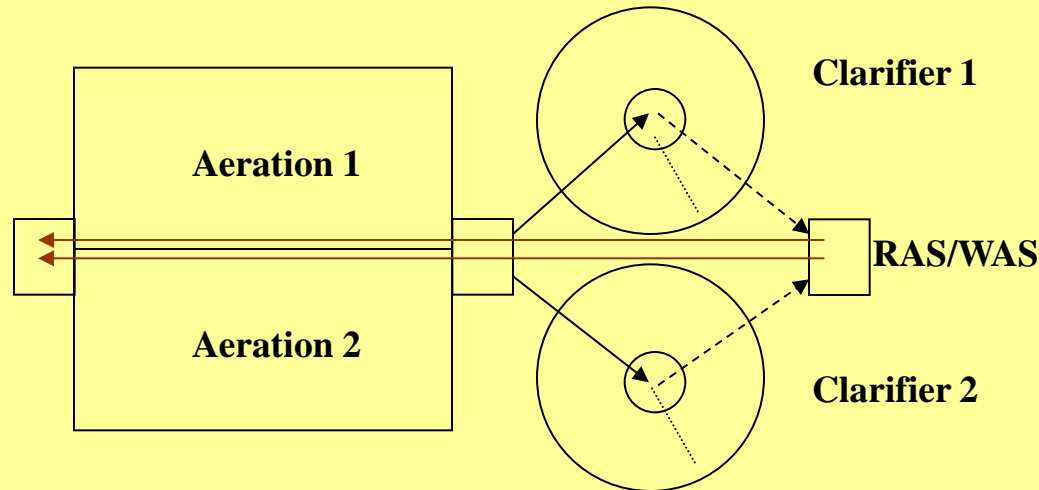
Simultaneous phosphorous removal

PLC control:

Fully automated process

Process modification simply change process timing

SBR disadvantages



When SBR equipment failure:

Repair “urgent” - no “by-pass”

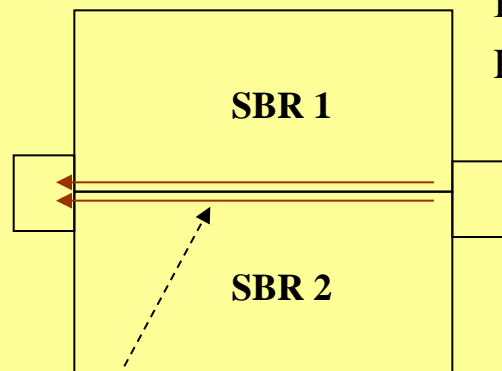
Replacement aeration devices - more complicated

Downstream equipment bigger:

2 hours of feed is released in 1 hour or less

Operator PLC control:

- panic when “faults”;
- blur on batch processes;
- Technician - re-trained PLC literate;



No RAS

(depends, required if long tank)

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SBR (Sequencing Batch Reactor) has emerged as an alternative to continuous flow activated sludge systems with following reasons:-

- Advent of PLC;
- Small land area requirements;
- Less unit processes; less capital & O&M cost;
- Less labor: automated control by PLC's;
- Batch: equalized variation and shock load (hydraulic & organic);
- Improve effluent quality: quiescent settling;
- Many parameters removal in a batch processes;

Since then, variation from the original fill and draw SBR system.....

Variation of SBR Designs

SBR: Anoxic / Anaerobic / Mixed Fill


Fill					
React					
Settle					
Decant					

SBR: Settle-Decant Fill

Fill					
React					
Settle					
Decant					

SBR: Fill-Aerate

Fill					
React					
Settle					
Decant					

 Variation of time fill & aeration

SBR: Intermittently Decanted EA

Fill					
DAT					
IAT					
Settle					
Decant					

SBR: Continuous Fill

Fill					
React					
Settle					
Decant					

Note:

Some with RAS or internal recycle from back to inlet zone to improve F_o/X_o

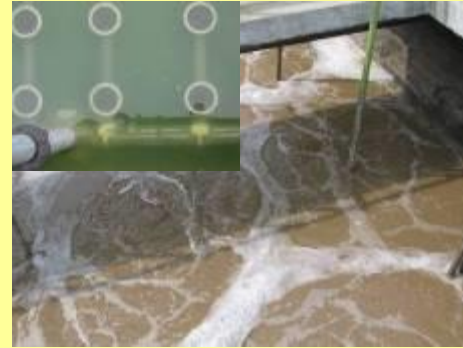
Decanter:-

- Surface skimming decanter (arm drive or floating);
- Siphon lock fixed position decanter;
- Fixed points actuator controlled decant valves;
- Floating weir decanter



Aeration Devices: -

- Diffuser system
(coarse or fine in tube or disc diffusers);
- Jet aerators, ejectors, or submersible aerators;
- “Sinkair” aerator, and floating aerators.



PLC system: -

- Different brand and different programming languages used;
- Hand wire with timer;



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Reviewed of SBR System:

- Looked at emergence of SBR: advent of PLC & controllable components & its beneficial uses;
- Described SBR process & its cycle charts;
- Identified various design considerations;
- Provided recommended design parameters;
- Evaluated benefits and draw backs of SBR system;
- Outlined variation of SBR by processes and by equipment;

In summary:

- SBR alternatives to continuous flow system;
- Variation in processes & equipment emerges must be evaluated;
- Its transient design parameters must be adopted carefully;
- Advantages and disadvantages of the system must be reviewed in an overall view dependence on types of application, operations and control requirement.